

24th Sept, 2019

To,

The Member Secretary

Karnataka State Pollution Control Board, "Parisara Bhavan", #49, 4th & 5th Floor, Church Street, Bangalore-560001

Dear Sir,

Sub: Submission of Environmental Statement Report (Form-V) (April, 2018 to March, 2019) for Grasilene Division, at Kumarapatnam – 581 123, Dist: Haveri Karnataka by M/s. Grasim Industries Ltd.

With reference to the aforesaid subject, we are herewith submitting the **Environmental Statement Report (Form-V)** for Grasilene Division, at Kumarapatnam – 581 123, Dist: Haveri Karnataka for financial year April, 2018 to March, 2019.

Thanking you with regards,

For GRASILENE DIVISION

(Ashok K Prabhakaran)

Vice president (Technical)

encl. a.a

Cc: The Environmental Officer,
Karnataka State Pollution Control Board,
"C" Block, Plot No. 501, Near Income Tax Office,
Devraj Urs Layout,
Davangere – 577 006.





Birla Cellulose Fibres from Nature

Grasim Industries Limited
Units: Harihar Polyfibers & Grasilene Division
Kumarapatnam 581123, Dist. Haveri, Karnataka.
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Regd. Office : P.O. Birlagram, Nagda 456 331 (M.P.)

FORM-V (See Rule 14)

Environmental Statement for the financial year ending the 31st March, 2019

PART-A

(I) Name and address of the owner/occupier of the Industry, operation or process Sr

Ajay Kumar Gupta Sr. President,

Grasim Industries Limited,

Grasilene Division,

Kumarapatnam - 581 123

Dist. Haveri., Karnataka.

(ii.) Industry category Primary - (STC Code)

Secondary - (SIC Code)

(iii) Production capacity (Units) 87,600 TPA of Viscose Staple Fibre

75110 TPA of Sulphuric Acid

14365 TPA of CS2 (Carbon Di-Sulphide) 69205 TPA of by-product Sodium Sulphate

20 MW Power Plant

1977

(iv) Year of establishment

(v) Date of the last Environmental Statement

submitted

29th September, 2018

PART-B

Water and Raw material consumption

(1)	Water Consumption	m³/day	15777
	Process	ж	11182
	Cooling	п	4380
	Domestic	in .	215

Name of Products	Process water consumption per unit of Product output		
	During the previous	During the current	
	financial year	financial year	
	2017- 2018	2018 - 2019	
(1) Viscose Staple Fibre (Semi-Synthetic)	61.0 m³/Ton	65.49 m³/Ton	
(2) -			
(3) -			

(ii) Raw Material consumption

* Name of raw materials		Name of products	S Consumption of raw material per unit of out p		
			During the previous financial year 2017 - 2018	During the current financial year 2018 - 2019	
a)	Rayon Grade Pulp	Staple Fibre	1.003	1.001	
b)	Caustic Soda	11	0.535	0.515	
c)	Sulphuric Acid	"	0.720	0.696	
d)	Carbon-di-Sulphide	11	0.159	0.160	
e)	Zinc	II .	0.0017	0.0015	
f)	Non-Ferric Alum		Nil	Nil	

^{*} Industry may use codes if disclosing details of raw materials would violate contractual obligations, otherwise all Industries have to name the raw materials used.

PART - C

Pollution discharged to environment, unit of output (Parameters as specified in the consent issued)

(1)	Pollutants	Quantity of Pollutants discharged (Mass/day)	Concentrations of pollutants in discharges	Percentage of variations from prescribed standards with reasons
a)	Water		Refer Annexure - I	
b)	Air		Refer Annexure - II	

PART - D Hazardous Wastes

(as specified under Hazardous & Other wastes/Management & Transboundary movement Rules, 2016)

Total Quantity (Kg)		
During the previous	During the current financial year	
2017 - 2018	2018 - 2019	
3900	2400	
Nil	Nil	
	During the previous financial year 2017 - 2018	

PART - E

Solid Wastes

		Total	Quantity (Kg)
		During the	During the current
		previous	financial year
		financial year	
		2017-18	2018 - 2019
a)	From Process	Nil	Nil
b)	From Pollution Control facilities		
	- Fly Ash *	150.21 Tons/day (Approx.)	111.13 Tons/day (Approx.)
c)	1) Quantity recycled or reutilised within Unit	Nil	Nil
	2) Sold	-	-
	3) Disposed	150.21 Tons/day	111.13 Tons/day
		(Approx.)	(Approx.)

^{*} The quantity includes Bottom ash also as per Fly Ash Notification S.O. 2804(E) dated 03.11.2009

PART - F

Please specify the characterisations (in terms of composition and quantum of Hazardous as well as Solid Wastes and indicate disposal practice adopted for both these categories of wastes

Refer Annexure - III

PART - G

Impact of the Pollution abatement measures taken on conservation of natural resources and on the cost of production

Refer Annexure - IV

PART - H

Additional measures/investment proposal for environmental protection including abatement of pollution, prevention of pollution

Refer Annexure - V

PART - I

Any other particulars for improving the quality of the Environment

Refer Annexure - VI

Annexure - 1 Ref.Part(C)1(a)

Pollution discharged to environment, unit of output (Parameters as specified in the consent issued)

SI.	Parameter	Unit	Limit Specified by	Quantity of	Conc. of	Percentage of
No.			KSPCB	pollutants discharged	Pollutants in mixed	variations from prescibed
				(Tons/Day)	discharges	tolerance limits
1.	Colour & Odour	-	All efforts should be made to remove colour & unpleasant odour as far as practicable		*	All parameters are maintained within the prescribed tolerance limits
2.	Suspended Solids	mg/l	Max.100	1.68	51	
3.	Dissolved Solids	"	Max.2100	60.18	1825	
	(Inorganic)					
4.	Temperature	°C	Shall not exceed 5°C above the receiving	1	33.0	
			water temperature	-		
5.	рН	-	6.0 - 8.5		7.4	
6.	Oil and Grease	mg/l	Max. 10.0	0.043	1.33	
7.	Biochemical Oxygen	"	Max.30.0	0.66	20	
	Demand (3 days, 27°C)					
8.	Chemical Oxygen Demand	"	Max.250.0	5.70	173	
9.	Mercury (as Hg)	"	Max. 0.01	-	ND	
10.	Total Chromium (as Cr)	"	Max.2.0	-	ND	
11.	Hexavalent Chromium (as Cr ⁺⁶)	"	Max.0.10	-1	ND	,
	Zinc (as Zn)	"	Less than 1.0	0.0026	0.08	
13.	Sulphate (as SO₄)	"	Max.1000	27.37	830	
14.	Sulphide (as S)	"	Max.2.0	0.045	1.38	
15.	Phenolic Compound (as C ₆ H ₅ OH)	"	Max.1.0	-	ND	
16.	Bio - assay (as per IS 6582-1971)	% Surv- ival	Not less than 90 % of test animal shall survive in 96 Hrs. test.The test shall be conducted as per IS 6582-1971		100 % Survival in 100 % Effl.	
17	Effluent volume	m3/d Max	48120		32975	

All possible efforts are made to remove colour and odour at source as far as possible.

ND Not Detectable

Note: Total volume of effluent discharge excluding the followings.

- 1) DM water used for boiler in both HPF and GRD is 3103 m3/day
- 2) Treated effluent used for greenery development and formers for irrigation purpose is 1540m3/day.

Annexure - II Ref. Part (C) I(b)

Pollution discharged to environment/unit of out put (Parameters as specified in the Consent issued

SI. No.	Parameter	Unit	Limit Specified by KSPCB	Quantity of Pollutants discharged (Tons/Day)	Conc. of Pollutants in discharges	Percentage of variations from prescribed tolerance limits
1.	Spinning Plant					
	a. SPM	mg/Nm³	150	0.159	21.5	Within the prescribed limits
	b. CS ₂	Kg/Ton	99	22.50	93.4	"
2.	H₂SO₄ Plant					
	a. SO ₂	Kg/Ton	1.0	0.130	0.54	"
	b. Acid Mist	mg/Nm³	50.0	0.0084	23.4	"
3.	Power Plant					
	CFBC Boiler					
	SPM	mg/Nm³	150	0.98	61	n

Annexure - III Ref. Part (F)

<u>Characterisations (in terms of composition and quantum) of Solid wastes and indicate</u> <u>disposal practice adopted for both these categories of wastes</u>

A Hazardous waste

Source	Nature	Quantity kg/d (approx.)	Mode of Disposal
Used oil generated from industrial operations using oil as lubricants in hydarulic systems or other application.	-	8.0-11.0	Sold to authorised oil recycler

B. Solid wastes

SI. No.	Source	Composition	Quantity t/d (approx.)	Mode of Disposal
1	Ash from Power Plant	Ash	150 - 180	Made available to cement manufacturers and brick manufacturers
2	CS2 Plant	Charcoal churi/ waste	3.5 - 4.5	Used as fuel in boilers
		Sulphur hardmass	0.15 - 0.20	Burnt in CFBC Boiler
3	ETP sludge (Organic)	Calorific value >3100 kcal/kg	4.0 - 5.0	Used as fuel in boilers after drying in sludge dryers
3	Gypsum sludge in ETP	CaSO4	5.0 - 8.0	Sold out to Cement Block Manufacturers

Annexure - IV Ref. Part (G)

Impact of the pollution abatement measures taken on conservation of natural resources and on the cost of production

Sheet 1/3

		Sileet 1/3
SI. No.	Control measures adopted	Impact on conservation of resources
1.	Reuse of Xanthator cleaning water	Water conservation and waste load reduction.
2.	Continuous Filters in place of Plate & Frame Presses for viscose preparation.	Chemical conservation and waste load reduction.
3.	Reuse of Pump Gland leakages in Soda Station.	Chemical conservation and waste load reduction.
4.	Recycling of Sumpzone in Cutter Ventury.	Water and Steam conservation.
5.	Condensate from sodium Sulphate Dryer reused in Spinning Cutter Ventury.	Water and Steam conservation.
6.	Reuse of condensate, dryer condensate and PHE cooling water from Acid Plant in Aftertreatment.	
7.	Use of Bleach wash in Desulph zone in Aftertreatment	Water conservation .
8.	Introduction of Multi Stage Flash evaporators	- Energy conservation.
	in place of Triple Effect Evaporators.	- Enhanced sodium sulphate recovery
9.	Introduction of Acid Absorption Crystallisers in place of Horizontal Continuous Crystallisers for recovery of Sodium Sulfate.	
10.	Introduction of mechanical seals in anhydrous circulation pumps, strong acid pumps and spin bath pumps to avoid gland leakages.	
11.	Entrainment Separator in MSFE	Chemical conservation and waste load reduction.
	Introduction of Settling & Pumping pit for	
	Power Plant drain to reuse the wastewater for coal quenching and handling plant	- Reduction in effluent discharge
13.	Reuse of CS2 condenser water for fibre wash	- Water conservation.
	in Aftertreatment section	- Reduction in effluent discharge
14.	Installation of Plate and heat Exchanger ipo Trombone Cooler for acid cooling. The hot water generated used fro fibre washing in Aftertreatment	Water conservation. Reduction in effluent discharge
15.	Use of part of sumpzone (high acidity stream) i.p.o fresh water for tow washing	Reduction in - Water consumption. - Effluent discharge - SO4/TDS concentration in treated effluent.
16.	Use of Multi Stage Flash Evaporator (MSFE) condensate for spin bath filter washing i.p.o fresh water.	1

		Sheet 2/3
SI. No.	Control measures adopted	Impact on conservation of resources
17	Installation of two additional Multi Stage Flash evaportaors to recover Sodium Sulpahte from lean streams	
18	Replacement of small capacity Spinning viscose storage tanks (16 Nos.) with continuous spinning tanks with stirrer	Reduction in - Cleaning frequency of tanks - Water consumption for tank cleaning - Organic load on ETP through reduced viscose loss
19	Recycling and reuse of treated effluent for a) Washing of Tow. b) Cleaning in CS2, H2SO4, ETP dept. etc. c) Lime Slurry preparation in ETP. d) Ash quenching in Power Plant. e) Fire fighting. f) spinning machine sides	Water conservation .
20	Replacement of M.S Aerator by S.S Aerator in Biological reactor	- Energy conservation
21	Condensing system for recovery of entrapped CS2 in Tow in Spinning department.	- Chemical conservation
22	Diffused aeration based secodary treatment system for effluent treatment	- Energy conservation
23	Exhaust System in Spinning Hall and Spin Bath Section.	Improved work environment
24	Replacement of Maurer Sieve band Slurry Press by Twin Roll Slurry Press	- To avoid chemical spillages - Reduction in waste load
25	Replacement of manual bin handling by Silo dumping system and pneumatic conveying instead of Belt conveying system	
26		 Increased productivity. Reduced downtime Human intervention minimised Reduced leakage/spillage of viscose and hence reduced influent load
27	Replacement of loose pulp Double Belt Conveyor by Pneumatic Conveyor	- Increased productivity Reduced pulp spillage - Reduction in influent load
28	Addition of additives in alkcell for improved quality of alkcell	Better xanthation resulting in reduced CS2 consumption
29	Marginal increase in spinning machine speed to reduce CS₂ loss	Improved CS2 recovery
30	Use of water in place of steam in cutter funnel to reduce CS₂ loss	Improved CS2 recovery
31	Modified hole configuration with Hastelloy C pipes in place of lead pipes for better steam penetration & CS ₂ expelling in Recovery Trough	
32	Modified scrubber for improving the vapour contact in CS ₂ recovery system	Improved CS2 recovery

SI. No.	Control measures adopted	Impact on conservation of resources
33	Bigger capacity first and second condenser with outer jacket in first condenser	
	Installation of automatic temperature control system for CS ₂ recovery	
35	Installation of efficient Circulating Fludised Bed Combustion (CFBC) Boilers with Distributed Control System (DCS) and better designed ESP	- Natural resource conservation
36	Construction of 175 m new Spinning Plant Chimney i.p.o 125 m Chimney (Main Stack)	For improved Ambient Air Quality.
37	Construction of 110 m new Power Plant Chimney i.po 78 m Chimney	
38	Installation of new acid plant with Double Conversion Double Absorption (DCDA) system.	To reduce SO2 emission per ton of Acid produced.
39	Demister Pads in Acid Absorption Tower of Acid Plant.	
40	Scrubbers for Acid Plant Chimney	SO2 emission per ton of Acid produced is less than the prescribed norms.
41	Klaus Kiln Sulphur Recovery Plant	To recover Sulphur from CS2 Plant tail gases.
42	Oil Scrubber system in CS ₂ Refinery	To minimise the CS2 concentration in CS2 Plant tail gases.
43	Scrubber for Deashing gas for CS2 Furnaces.	Improved work environment.
44	Closed Calciner for Charcoal Calcination in place of Open Calciners.	Improved work environment.
45	Scrubbers for Exhaust air from salt Scrubber	Improved work environment.
46	Electro Static Precipitators for Power Plant Boilers	Low SPM emission.
47	Installation of Belt Press in place of Vacuum Belt Filter	Increasing the dry content of sludge
48.	Installation of Filter Press for ETP sludge handling	
49.	Dryers for ETP sludge	Dried sludge used as fuel in boilers after mixing with coal.
50.	Usage of fly ash for brick and cement manufacturing	Reuse of solid waste
51	Installation of VFD for main drive & soft finish drive in M/c No. 1 & 2	
52	Preheating of Demin water in power plant with MSFE condensate.	
53	Installation of diffusers in place of surface aerators in old biological reactor.	Conserve electricity and to improve the quality of treated effluent

Impact on Pollution Control measures on cost of production can not be exactly quantified as there are other steps being taken continuously like inpaint improvements, close supervision, Wastage Control etc. which have bearing on cost of production.

Annexure - V Ref. Part (H)

Additional investment proposal for Environmental protection including abatement of Pollution, Prevention of Pollution

SI.	Projects	
No.		
1.	Degasser For M/c#3 for CS2 & H2S reduction in Spin bath	
2.	Bigger size RVF to improve productivity thereby reduction in water, steam & power consumption	
3	Installation of on/off valves in Spin bath feed line to Machine for eliminating spin bath loss	
4	Installation of centrifuge system (2 Sets) in place of Plate and frame filter press for Reject viscose filtration for reducing Pulp & Caustic loss	
5	Replacement of existing Centrifugal Chiller with Once through system for cooling Mix charge system for Power saving	
6	Replacement of inefficient Flash Deaerator Condenser Pump #1 for Power saving	
7	Replacement of inefficient Condenser Pump #4 of Cooling Tower # 5 in Viscose for Power saving	
8	Installation of Booster pump for MSFE#1 to 2 for improving Specific steam consumption	
9	Conductivity meter for individual MSFE condensate for Minimising Spin bath losses	
10	Replacement of inefficient Chilled water Pump #1 & 2 in CS2 /H2SO4 Department for Power saving	
11	SOX, NOX And CO analyzer for AFBC Boiler	